



ProEcoPolyNet

ProEcoPolyNet Best practice Sheet

'Annex 42: Fuel Cell CHP'

RTD Project Identification

RTD Project Name: FC+COGEN-SIM:
IEA/ECBCS Annex 42 - The Simulation of
Building-Integrated Fuel Cell and Other
Cogeneration Systems

RTD Contract No.: IEA/ECBCS Annex 42

Programme: Annex 42 operates under the
auspices of the International Energy Agency's
(<http://www.iea.org>) Energy Conservation in
Community Systems (<http://www.ecbcs.org/>)
program

Description of technology

Annex 42 considers modelling of various
cogeneration technologies in the building
environment. This Best Practice Sheet focuses
on Fuel Cell CHP.

In a fuel cell, the chemical reaction of
combustion is made using an electrochemical
reaction where the reactants are separated by
a tight membrane that only allows ions
crossing. To complete the electrical balance,
electrons have to move through a circuit, which
produces a current. Depending on the type of
membranes, the ions that will cross the
membrane will be different: H⁺ for PEMFC or
O²⁻ in SOFC.

Proton Exchange Membrane Fuel Cell
(PEMFC) technology involves the reaction of
hydrogen with oxygen in the presence of an
electrolyte to produce electricity without
combustion and mechanical work. Water and
heat are produced as by-products. The
reaction is achieved through the
electrochemical oxidation of a fuel (hydrogen)
and the electrochemical reduction of oxygen.
The following equations illustrate the
electrochemical reactions:

Anode: $H_2 \rightarrow 2H^+ + 2e^-$

Cathode: $2H^+ + \frac{1}{2}O_2 + 2e^- \rightarrow 2H_2O$

Total Reaction: $H_2 + \frac{1}{2}O_2 \rightarrow H_2O$

The amount of electricity that can be produced
by the reaction is limited by the Gibbs free
energy the remaining enthalpy of reaction is
converted into heat. Furthermore, in order to
maintain a sufficient driving force for the ions
transfer through the membrane, the

combustion can not be complete, the
remaining fuel will be burned in an afterburner
that will produce heat useful for cogeneration.
The temperature of operation of the fuel cell
has to be controlled according to the
membrane specification. Therefore, the
released heat can be harnessed for space and
domestic hot water heating for residential,
commercial or institutional applications. The
hydrogen used as fuel can be produced from
different sources such as natural gas, propane,
coal, or through the electrolysis of water.

A fuel cell system consists of several
subsystems, which include the fuel cell
processor (i.e. hydrogen reformer), fuel cell
stack, auxiliary systems required for operation
and the inverter. The process of producing
hydrogen from a fuel source such as natural
gas is called reforming, and the process can
either be internal reforming or external
reforming depending on the type of fuel cell.
The general design of most fuel cells is similar
except for the type of electrolyte used.
Currently, there are various types of fuel cell
technologies in different stages of
development. These include alkaline fuel cells
(AFC), polymer electrolyte membranes (PEM),
phosphoric acid fuel cells (PAFC), molten
carbonate fuel cells (MCFC), solid oxide fuel
cells (SOFC), and lately, direct methanol fuel
cells (DMFC). Amongst these, PEM and SO
fuel cells have the highest potential for the
residential sector.

Operating principle

The performance of fuel cell systems is a
function of the type of fuel cell and its capacity.
The optimization of electrical efficiency and
performance characteristics of fuel cell
systems poses an engineering challenge
because fuel cell systems are a combination of
chemical, electrochemical, and electronic
subsystems²⁵. Due to the several subsystem
components of a fuel cell system laid out in
series, the electrical efficiency of the system is
a multiple of the efficiencies of the individual
sections. The factors determining the electrical
efficiency of a fuel cell include the fuel cell
efficiency, the fuel conversion and the non

converted fuel processing. The electrical efficiency is expressed by the ratio between the net electricity produced and the fuel consumed. The system efficiency is influenced by the quality of the system integration, for example the use of the depleted fuel to satisfy the energy requirement of the fuel processing.

Technical characteristics and operational data

Fuel Cell Type	PEMFC	PEMFC	PAFC	SOFC	MCFC
Nominal Electricity Capacity (kW)	10	200	200	100	250
Electric Heat Rate (MJ/kWh), HHV	12	10.3	10	8	8.4
Electrical Efficiency (%) HHV	30	35	36	45	43
Fuel Input (MJ/hr)	105	2,110	2,005	845	2,110
Operating Temperature [°C]	70	70	200	950	650
Cogeneration Characteristics					
Heat Output (MJ/hr)	42	760	780	200	465
Heat Output (kW equivalent)	13	211	217	56	128
Total Overall Efficiency (%) HHV	68	72	75	70	65
Power/Heat Ratio	0.77	0.95	0.92	1.79	1.95
Net Heat Rate (MJ/kWh)	6.7	5.5	5.1	5.5	6
Effective Electrical Efficiency (%) HHV	53.6	65.0	70.3	65.6	59.5

In both power generation and cogeneration applications, fuel cell systems have excellent load following characteristics. Fuel cell stack efficiency improves at lower loads, resulting in an increase in system electrical efficiency that is relatively steady down to one-third to one-quarter of rated capacity

Location and use

- ▶ *Private Buildings*
- ▶ *Residential Buildings*
- ▶ *Commercial Buildings*
- ▶ *Public Buildings*
- ▶ *Others*

Capital investment and maintenance costs

Fuel Cell Type	PEMFC	PEMFC	PAFC	SOFC	MCFC
Nominal Electricity Capacity (kW)	10	200	200	100	250
Variable Service Contract (\$/kWh)	0.0121	0.0087	0.0087	0.0102	0.0072
Variable Consumables (\$/kWh)	0.0002	0.0002	0.0002	0.0002	0.0002

Fixed (\$/kW-yr)	18.0	6.5	6.5	10.0	5.0
Fixed (\$/kWh @ 8,000 hrs/yr)	0.0023	0.0008	0.0008	0.0013	0.0006
Stack Fund (\$/kWh)	0.0188	0.0132	0.0193	0.0125	0.0350
Stack Life (yrs)	4	4	5	8	4
Recovery Factor (%)	50	35	30	20	30
Net O & M cost (\$/kWh)	0.033	0.023	0.029	0.023	0.043

▶ Maintenance

Fuel cells have the potential for very low maintenance costs because they have fewer moving parts when compared to reciprocating engines and micro-turbines. However, maintenance of ancillary systems such as pumps and fans needed for operating fuel cell systems can increase maintenance costs. In addition, these ancillary systems can cause an increase in both scheduled and unscheduled downtime

The maintenance cost for the commercially available PAFC systems (200 kW) including an allowance for periodic stack replacements is from 0.02 - \$5 \$/kWh (0.016 – 3.92 €/kWh). It is assumed that the higher costs have been obtained from laboratory trials. Periodic stack replacement alone for the commercially available 200 kW PAFC fuel cell is estimated to be around 0.0193 \$/kWh (0.0151 €/kWh). The cost to replace a 10kW PEM fuel cell stack is estimated to be 0.0188 \$/kWh (0.0147 €/kWh), while the estimated cost to replace a 200kW PEM fuel cell stack is 0.0132 \$/kWh (0.0104 €/kWh), and 0.0125 \$/kWh (0.0098 €/kWh) to replace a 100 kW SOFC fuel cell stack

State of Development/Market implementation

- ▶ *Prototype*
- ▶ *Field tested*
- ▶ *Demonstration*

CO₂ and primary energy savings

Fuel Cell Type	PEMFC	PEMFC	PAFC	SOFC	MCFC
Nominal Electricity Capacity (kW)	10	200	200	100	250
Electrical Efficiency (%) HHV	30	35	36	45	43
Emissions Characteristics					
NO _x [g / MWh]	27	27	14	23	27
CO [g / MWh]	32	32	23	18	18
Unburned Hydrocarbons [g / MWh]	5	5	5	5	5
CO ₂ [kg / MWh]	617	531	515	413	431
Carbon [kg / MWh]	168	143	141	111	118

Notes: Emissions adjusted to 15% oxygen. Emissions do not account for cogeneration operations.

Benefits and obstacles

The advantages of fuel cell cogeneration systems include low noise level, potential for low maintenance, excellent part load management, low emissions, and a potential to achieve an overall efficiency of 85-90% even with small units. Stationary power fuel cells typically burn natural gas, and release fewer environmentally harmful emissions than those produced by a combustion cogeneration plant. With a fuel cell, carbon dioxide emissions may be reduced by up to 49%, nitrogen oxide (NOX) emissions by 91%, carbon monoxide by 68%, and volatile organic compounds by 93%. Low emissions and noise levels make fuel cells particularly suitable for residential, commercial and institutional applications. However, the high cost and relatively short lifetime of fuel cell

systems are their main drawback. Ongoing research to solve technological problems and to develop less expensive materials and mass production processes are expected to result in advances in technology that will eventually reduce the cost of fuel cells.

Contact and further information

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Date of Elaboration: 24/10/2007